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98310768.1 29 December 1998 (29.12.98) EP(71) Applicant (for all designated States except US): SHELL
INTERNATIONALE RESEARCH MAATSCHAPPIJ B.V.
[NL/NL]; Carel van Bylandtlaan 30, NL-2596 HR The
Hague (NL).

(72) Inventors; and

(75) Inventors/Applicants (for US only): WENTINCK, Hendrik,
Martinus [NL/NL]; Badhuisweg 3, NL-Amsterdam 1031
(NL). SMIT, Jacobus, Antonius, Jozef [NL/NL]; Bad-
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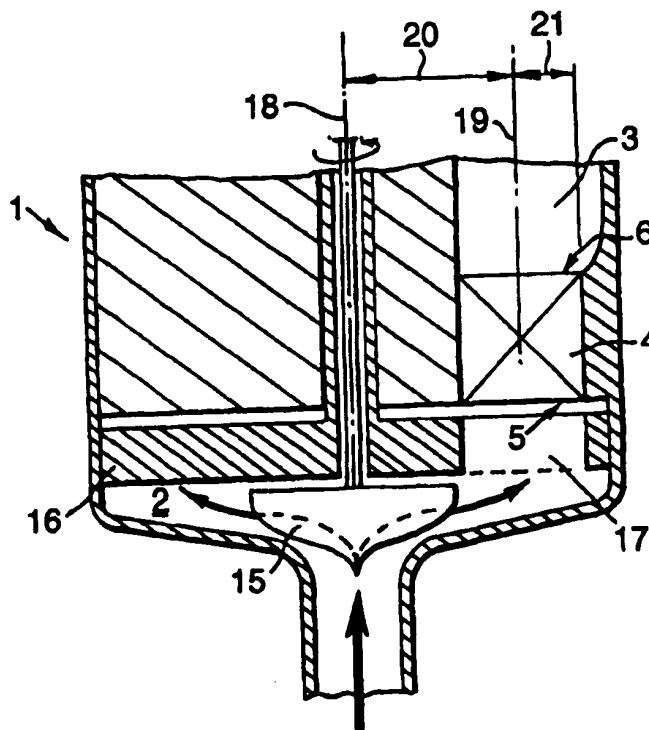
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(54) Title: CATALYTIC REACTOR

(57) Abstract

The invention relates to a reactor (1), suitable for the catalytic conversion of a feed mixture which is capable of explosion and/or ignition, comprising a feed supply chamber (2), an effluent discharge chamber (3), a catalyst bed (4) having an upstream surface (5) and a downstream surface (6) which is in fluid communication with the effluent discharge chamber (3), and means for covering part of the upstream surface (5) that partly confine the feed supply chamber (2), wherein the feed supply chamber (2) has, during normal operation, no zones where the fluid flow is stagnant, to the use of such a reactor (1), in particular a catalytic partial oxidation process, and to transport means provided with such a reactor (1).



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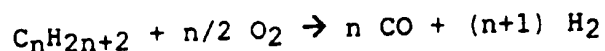
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CATALYTIC REACTOR

The present invention relates to a reactor wherein part of the upstream surface of the catalyst bed can be covered, to the use of such a reactor in a process for the catalytic conversion of a feed mixture which is capable of ignition or explosion, and to transport means provided with the reactor.

An example of a process for the catalytic conversion of a feed mixture which is capable of ignition or explosion is the catalytic partial oxidation of hydrocarbonaceous feedstocks, in particular hydrocarbons. The partial oxidation of paraffinic hydrocarbons is an exothermic reaction represented by the equation:



There is literature in abundance on the catalysts and the process conditions for the catalytic partial oxidation of gaseous hydrocarbons, in particular methane. Reference is made, for instance, to EP-A-303 438, US-A-5,149,464, and International patent application WO 92/11199.

The hydrogen produced by the catalytic partial oxidation process of hydrocarbonaceous feedstocks can suitably be used as feed for a fuel cell. In fuel cells, hydrogen and oxygen are converted into electricity and water. Fuel cell technology is well known in the art.

One of the most challenging applications of fuel cells is in transportation. Transport means, such as automotive vehicles and crafts, powered by fuel cells are under development. The oxygen needed for the fuel cell may be obtained from the ambient air, the hydrogen feed could be obtained from a hydrogen fuel tank but is preferably produced on-board, for example by catalytic

reforming of methanol. The on-board production of hydrogen by catalytic reforming of methanol has been proposed, for example by R.A. Lemons, Journal of Power Sources 29 (1990), p 251-264.

5 Recently, the on-board production of hydrogen by a catalytic partial oxidation process, for example as described in WO99/19249 has been proposed as an alternative for steam reforming of methanol. An important advantage of this catalytic partial oxidation process is
10 its flexibility towards the choice of fuel.

 It is important for a power system in transportation applications, that it is able to vary the power output with a factor of at least about 60, preferably of at least 100. Several systems for controlling the power
15 output of fuel cell systems for transportation applications are under development. In US 5,771,476, for example, a system for controlling the power output of a fuel cell is disclosed, wherein the supply of a reactant gas, such as air, to the fuel cell unit is controlled.

20 Alternatively, in the case of a fuel cell system having an on-board hydrogen-producing unit, the power output may be controlled by regulating the quantity of hydrogen produced. In a catalytic conversion process, the amount of hydrogen produced is directly proportional to
25 the moles of feed mixture that are converted, provided that the process conditions and the composition of the feed mixture are kept constant.

 If the supply of feed mixture to a catalyst bed would be varied in the range between the minimum amount desired
30 and up to 60 times that amount, large variations in superficial velocity, residence time, and pressure of the feed mixture would occur. These large variations may result in problems, especially at the lowest feed throughput. Especially in the case of a feed mixture that
35 is capable of explosion and/or ignition, such as in the

catalytic conversion of a mixture of hydrocarbons and an oxygen-containing gas, the low superficial velocity of the feed mixture at low throughputs could result in a residence time of the feed mixture upstream of the catalyst which is greater than the auto-ignition delay time, thus causing auto-ignition or particle induced ignition, and in flash-back of flames from the catalyst bed.

It is known to achieve a large variations in output by using a plurality of catalytic reactors, each containing a catalyst provided with a feed supply system, and varying the number of reactors which are turned on, whilst keeping the feed throughput per reactor essentially constant. It will be appreciated that such multi-reactor systems are relatively expensive, since a plurality of feed supply systems, including the flow control equipment, are needed. Moreover, in such a system the output can only be varied stepwise and not continuously. Therefore, there is a need in the art for catalytic reactors that can achieve large variations in output in a single reactor.

It is also important that the reactor comprises a cooling system that is capable of dealing with a varying throughput of hot conversion product, such as hot synthesis gas in the case of a catalytic partial oxidation process. Suitably, the hot conversion product can be cooled by heat exchanging it against air or air/steam mixtures in flexible corrugated metal tubes. Such tubes are known and commercial available, for example from Witzenmann GmbH in Germany. The use of these tubes as heat exchanger is described in EP-A-298 369. Because of their flexibility, the tubes can accommodate thermal stresses due to a varying throughput of hot conversion product.

In view of the above, the problem to be solved is how to achieve, in a single reactor for the catalytic conversion of a feed mixture that is capable of explosion and/or ignition, a large variation in the quantity of conversion products by varying the throughput of the feed mixture, whilst avoiding uncontrolled gas-phase reactions, such as auto-ignition or particle induced ignition of the feed mixture upstream of the catalyst and flash-back of flames from the catalyst bed.

It has now been found that the above-mentioned problem can be solved by using a reactor wherein part of the upstream surface of the catalyst bed can be covered as a function of the throughput of feed mixture in such a way that, during normal operation, the space upstream of the catalyst bed, i.e. the feed supply chamber, has no zones wherein the fluid flow is stagnant. Reference herein to zones wherein the fluid flow is stagnant is to zones wherein the fluid is hardly exchanged with fluid from surrounding zones, resulting in a relatively long residence time of the fluid in that zone, i.e. relatively long compared to the average residence time of fluid in the feed supply chamber. Typically, the residence time of the fluid in zones wherein the flow is stagnant exceeds 5 times the average residence time of the fluid in the feed supply chamber.

Accordingly, the present invention relates to a reactor, suitable for the catalytic conversion of a feed mixture which is capable of explosion or ignition, which reactor comprises a feed supply chamber, an effluent discharge chamber, a catalyst bed having an upstream surface and a downstream surface which is in fluid communication with the effluent discharge chamber, and means for covering part of the upstream surface that partly confine the feed supply chamber, wherein the feed

supply chamber has, during normal operation, no zones where the fluid flow is stagnant.

5 The uncovered part of the upstream surface of the catalyst bed is in fluid communication with the feed supply chamber. In order to be able to achieve a sufficiently large variation in the quantity of catalytic conversion products, the ratio between the maximum and minimum value for the uncovered area of the upstream surface area is preferably at least 5, more preferable at
10 least 10, most preferably at least 20.

Reference herein to a catalyst bed is to a permeable fixed arrangement, for example a fixed bed of particles, a porous monolithic structure such as a ceramic or metal foam or honeycomb, or another permeable fixed
15 arrangement, such as arrangements comprising metal gauzes or wires. Alternatively, a single reactor may comprise more than one catalyst bed, for example a plurality of ceramic foams. In the case of a plurality of catalyst beds in a single reactor, reference to the surface of the
20 catalyst bed is to the total surface of all catalyst beds. Feed will be supplied at the upstream side of the catalyst bed, and after catalytic conversion of the feed into effluent, effluent will be discharged at the downstream side of the catalyst bed.

25 The feed supply chamber is defined as the space upstream of the catalyst bed wherein the reactants are supplied. This space is confined by the uncovered upstream surface of the catalyst bed, one or more surfaces of the means for covering part of the upstream
30 surface, and, optionally, one or more other surfaces of the reactor.

To avoid that, during normal operation of the reactor according to the invention, the feed supply chamber has zones where the fluid flow is stagnant:

- a) part of the upstream surface of the catalyst bed is covered in such a way that, at any setting of the means for covering part of the upstream surface, the shape of the feed supply chamber is such that no dead space(s) occur, i.e. during normal operation the fluid in the feed supply chamber is flowing in a plug flow regime; or
- b) the fluid in the feed supply chamber is forced to swirl.

A combination of a) and b) may be applied in order to avoid zones where the fluid flow is stagnant. It will be appreciated that the requirement to the shape of the feed supply chamber at each setting of the means for covering part of the upstream surface can be somewhat relaxed if, under normal operation, the fluid feed mixture is forced to swirl.

Thus, the feed supply chamber of the reactor of the invention is preferably equipped with means for swirling the feed mixture, preferably in tangential direction with respect to the central longitudinal axis of the catalyst bed. The means for swirling the feed mixture may be any suitable means, for example a fan, such as the fan of a compressor of a turbocharger.

In those embodiments of the reactor according to the present invention wherein, during normal operation, the shape of the feed supply chamber is such that the fluid in the feed supply chamber is flowing in a plug flow regime, it is required that the residence time of the feed mixture in the feed supply chamber is below the auto-ignition delay time and that the superficial velocity of the feed mixture at the upstream catalyst surface is high enough to prevent flash-back. The feed supply chamber may have a constant volume, i.e. a volume that is not varied as a function of feed throughput, provided that the volume is small enough to warrant that the residence time and the superficial velocity of the

feed mixture meet the above requirements at the smallest required feed throughput. It is preferred that the volume of the feed supply chamber is regulated as a function of the uncovered upstream surface area and feed throughput. More preferably, the volume of the feed supply chamber is regulated in such a way that the residence time of the fluid in the feed supply chamber is varied within a factor of at most 5, upon variations in feed throughput of a factor 60, and that the superficial velocity is typically kept above 1 m/s for the catalytic partial oxidation process described below.

The invention will now be illustrated in a non-limiting manner with reference to the schematic Figures 1 to 7. The Figures are not drawn to scale. Figures 1 to 7 each show a different embodiment of the present invention.

Figures 1 to 4 each show part of a longitudinal section of a reactor 1 according to the present invention, which reactor 1 is rotation symmetrical around central longitudinal axis C. Reactor 1 comprises a feed supply chamber 2, an effluent discharge chamber 3, a cylindrical catalyst bed 4, having an upstream surface 5 and a downstream surface 6, and means for covering part of the upstream surface 5 comprising a body 7 which is moveable parallel to the upstream surface 5. The body 7 has a first surface 8 directed to the upstream surface 5 and a second surface 9 partly confining the feed supply chamber 2. Reactor 1 further comprises a surface 11 which is partly confining the feed supply chamber 2. Figures 1 to 4 each show a position of the body 7 at which part of the upstream surface 5 of catalyst bed 4 is covered by the first surface 8 of body 7.

In all embodiments shown in Figures 1 to 4, the shape of the feed supply chamber 2 is such that, at any setting of the body 7 and thus at any size of the uncovered

upstream surface area, essentially no dead space(s) occur in the feed supply chamber. Thus, during normal operation, the fluid in the feed supply chamber is essentially flowing in a plug flow regime, i.e. without occurrence of substantial back mixing.

In order to avoid, at any setting of the means for covering part of the upstream surface, that the feed supply chamber has zones where the fluid flow is stagnant, it is preferred that the feed supply chamber has a flow defining surface having an angle with the upstream surface 5 of the catalyst bed 4 which is smaller than 70° , more preferably smaller than 60° , even more preferably smaller than 45° . Reference herein to a flow defining surface is to a surface that defines the direction of the flow since the fluid flow is deflected by the flow defining surface to the upstream surface of the catalyst bed. In the embodiments shown in Figures 1 and 2, the flow defining surface is referred to with reference numeral 11; and in Figures 3 and 4 with reference numeral 9. The angle between the flow defining surface and the upstream surface is referred to with reference numeral 12. In Figures 1 to 4, the angle 12 is about 20° .

It is preferred that the feed supply chamber further has a flow guiding surface that is substantially parallel to the flow defining surface. Substantially parallel must be construed as having an angle of not more than 15° with the flow defining surface, preferably not more than 10° , more preferably as having an angle of 0° . The embodiments of the reactor of the invention shown in Figures 1 and 3 comprise a feed supply chamber 2 having a flow guiding surface (surface 9 in Figure 1; surface 11 in Figure 3) that is parallel to the flow defining surface (surface 11 in Figure 1; surface 9 in Figure 3).

Although the shape of the feed supply chamber 2 of reactor 1 as shown in Figures 1 to 4 is such that no dead spaces would occur at any setting of the body 7, a means for swirling (not shown) the feed mixture may be advantageously applied.

Figure 5a shows a longitudinal section of part of a reactor 1 comprising three separate catalyst beds 4 (one of the three beds is shown), and means 15 for swirling the feed mixture in tangential direction. The means for covering part of the upstream surface 5 comprise a rotatable disc 16 having three openings 17 excentric to the axis of rotation 18 (one of the three openings is shown). In the embodiment of Figure 5, means 15 is the fan of a compressor of a turbocharger.

Both Figures 5b and 5c separately show the disc 16 and its position with respect to the upstream surfaces 5 of the three catalyst beds. Figure 5b shows the position of the disc 16 wherein the uncovered area of upstream surface 5 has its maximum value. Figure 5c shows the position of disc 16 wherein a large part of the upstream surface 5 is covered.

The axis of rotation 18 of disc 16 is parallel to and excentric with respect to the longitudinal axis 19 of any of the catalyst beds. The radius 20 of disc 16 is larger than the sum of the radius 21 of any of the catalyst beds and the distance between the longitudinal axis 19 and the axis of rotation 18 of disc 16. Preferably, the distance between the centre of the opening 17 and the axis of rotation 18 of the disc 16 is equal to the distance between the longitudinal axis 19 of the catalyst bed and the axis of rotation 18 of the disc 16, such as is the case in the embodiment of Figure 5.

It will be appreciated that in the reactor 1 as shown in Figure 5, during normal operation, zones where the

fluid flow is stagnant would occur in the feed supply chamber 2 if the feed fluid would not be forced to swirl.

Figure 6 shows an embodiment of the invention wherein the means for covering part of the upstream surface 5 comprises a flexible wall 22 having a surface 23 that partly defines the feed supply chamber 2 and is capable of partly covering the upstream surface 5 of the catalyst bed 4. Figure 6a shows the position of the flexible wall 22 wherein the uncovered area of the upstream surface 5 is maximum; Figure 6b shows a position of the flexible wall 22 wherein a part of the upstream surface 5 is covered by the surface 23. Suitable flexible walls may consist of any flexible high-temperature resistant material, for example a metal foil. Corrugated metal foils are particularly suitable.

In the embodiment of Figure 6, a means for swirling the feed mixture (not shown) may be applied.

In the embodiments shown in Figures 1 to 6, the same part of the upstream surface 5 of the catalyst bed 4 is exposed to the feed at low throughput. Thus, the part of the surface that is exposed at low throughputs will deteriorate or deactivate more quickly than the part that is only exposed at high feed throughput. Therefore, it is advantageous when the part of the upstream surface that is exposed at low throughput can be varied. This can, for example, be achieved by means of means for covering part of the upstream surface comprising two moveable bodies.

Figure 7a and 7b show a reactor 1 comprising a hollow cylindrical catalyst bed 4 having an upstream surface 5 at the inside of the cylindrical bed. The means for covering part of the upstream surface 5 comprise two bodies 24, 25 which are moveable parallel to the upstream surface 5. Bodies 24 and 25 are shown in more detail in Figures 7c and 7d, respectively. Both bodies have a first surface 26, 27 that is directed to the upstream surface 5

of the catalyst bed 4, and a second surface 28, 29 that is partly confining the feed supply chamber 2. Further, the body 25 comprises a flow defining surface 30 having an angle with the upstream surface 5 which is smaller than 70°. Both bodies 24, 25 are provided with projections 31,32 that can grip into each other. In the embodiment shown in Figures 7a and 7b, the projections are in the shape of saw teeth. Alternative shapes, however, may be applied. The uncovered area of the upstream surface 5 can be regulated by moving body 25 in the direction indicated by the arrow on body 25 in Figures 7a and 7b. The part of the upstream surface 5 that is uncovered at low throughput can be varied by moving body 24 in the direction indicated by the arrow on body 24 in Figure 7b. The embodiment shown in Figures 7a and 7b is preferable equipped with means (not shown) for swirling the feed mixture in order to avoid that the feed supply chamber 2 has zones where the fluid flow is stagnant.

In the reactor according to the invention, the distance between the covered upstream surface of the catalyst bed and the surface covering it is preferably such that flames cannot be sustained between the two surfaces. Suitably, this distance is not exceeding three times the quenching distance, preferably not exceeding one time the quenching distance. The quenching distance is defined as the distance within which two walls must be brought to prevent flash-back, i.e. flames cannot be sustained at this distance, they are quenched or extinct.

For a given laminar flame velocity and operating pressure, the quenching distance can be calculated by methods known in the art. The laminar flame velocity depends, among others, on the composition and temperature of the feed mixture. Estimation methods for the flame velocity are known in the art. For example, for a

5 catalytic partial oxidation process as described below,
with a oxygen-to-carbon ratio of about 0.5, performed at
a pressure of 6 bar (absolute), wherein the laminar flame
velocity of the feed mixture is about 0.5 m/s and the
temperature of the feed mixture just upstream of the
surface of the catalyst bed is about 500 °C, the
quenching distance is about 0.5 mm.

10 The means for covering part of the upstream surface
suitably consist of inert, high-temperature resistant
material, such as metals or refractory oxides. Metal
alloys, such as high-chromium steel alloys and feocralloy-
type materials are particularly suitable. The moveable
body or bodies may be moved with respect to the upstream
surface by any suitable means known in the art. The body
15 may be moved by means of the fluid flow.

The catalyst bed may have any suitable shape.
Preferably, the catalyst bed is a catalyst-containing
cylindrical arrangement, more preferably a circle
cylindrical arrangement, having an inner and an outer
20 surface. The upstream surface of the catalyst bed may be
either the inner or the outer surface of the cylindrical
arrangement, preferably the inner surface, since this
minimises the volume of the feed supply chamber and thus
minimises the risks for ignition and/or explosion.

25 In a further aspect the present invention relates to
a process for the catalytic conversion of a fluid feed
mixture which is capable of ignition or explosion,
wherein the fluid feed mixture is contacted with a
catalyst bed retained in the reactor as described
30 hereinbefore. In particular, the invention relates to a
process for the catalytic partial oxidation of a hydro-
carbonaceous feedstock, wherein a feed mixture comprising
the hydrocarbonaceous feedstock and an oxygen-containing
gas is contacted with a catalyst bed retained in the
35 reactor as described hereinbefore.

The hydrocarbonaceous feedstock suitably comprises hydrocarbons and/or oxygenates which are gaseous under the condition prevailing at the in the catalyst bed during normal operation. The feedstock may contain
5 compounds that are liquid and/or compounds that are gaseous under standard conditions of temperature and pressure (i.e. at 0 °C and 1 atm.). Oxygenates are defined as molecules containing apart from carbon and
10 hydrogen atoms at least 1 oxygen atom which is linked to either one or two carbon atoms or to a carbon atom and a hydrogen atom, such as alcohols, ethers, acids and esters.

The oxygen-containing gas may be air, substantially pure oxygen, or oxygen-enriched air, preferably air.

15 The feed comprises the hydrocarbon and/or oxygenate feedstock and the oxygen-containing gas in amounts sufficient to give an oxygen-to-carbon ratio in the range of from 0.3 to 0.8, preferably of from 0.45 to 0.75, more preferably in the range of from 0.45 to 0.65. If
20 oxygenate feedstocks are used, e.g. methanol, oxygen-to-carbon ratios below 0.3 can suitably be used. References to the oxygen-to-carbon ratio refer to the ratio of oxygen in the form of molecules (O₂) to carbon atoms present in the hydrocarbon and/or oxygenate feedstock.

25 The feed mixture may comprise steam and/or carbon dioxide. If steam is present in the feed mixture, the steam-to-carbon ratio (that is the ratio of molecules of steam (H₂O) to carbon atoms in the feedstock) is preferably in the range of from above 0.0 to 3.0, more
30 preferably of from above 0.0 to 2.0.

The catalytic partial oxidation process is preferably operated at a temperature in the range of from 750 to 1500 °C, more preferably in the range of from 800 to 1350 °C. Temperatures in the range of from 850 to 1300 °C
35 are particularly suitable. Reference herein to

temperature is to the temperature in the top (i.e. the upstream side) layer of the catalyst bed.

5 The catalytic partial oxidation process is preferably operated at a pressure in the range of from 2 to 100 bar (absolute), preferably in the range of from 3 to 50 bar (absolute), more preferably of from 5 to 30 bar (absolute).

10 In the catalytic partial oxidation process of the invention, the feed throughput, and thus the gas hourly space velocity (expressed as normal litres of gas per kilogram of catalyst per hour; normal litres are litres at STP, i.e. 0 °C and 1 atm.), is varied. At maximum feed throughput, i.e. typically at 0% coverage of the upstream surface of the catalyst bed, the feed mixture is
15 preferably provided at gas hourly space velocities which are in the range of from 20,000 to 10,000,000 Nl/kg/h, more preferably in the range of from 50,000 to 5,000,000 Nl/kg/h, even more preferably in the range of from 100,000 to 3,000,000 Nl/kg/h.

20 Catalyst compositions suitable for use in the catalytic partial oxidation process are known in the art. Such catalysts generally comprise, as active component, a metal selected from Group VIII of the Periodic Table of the Elements. References in this specification to the
25 Periodic Table of the Elements are to the CAS version, as published in the CRC Handbook of Chemistry and Physics, 68th Edition. Catalysts comprising, as the catalytically active component, a metal selected from rhodium, iridium, palladium and platinum are preferred. Catalysts
30 comprising rhodium or iridium are most preferred.

35 The catalytically active metal is most suitably supported on a carrier, such as refractory oxide particles, ceramic or metal monolithic structures, or metallic arrangements. Suitable carrier materials are well known in the art and include refractory oxides, such

as silica, alumina, titania, zirconia and mixtures thereof and metals such as high-alloy, alumina-containing steel, for example fecralloy-type materials.

5 The catalyst may comprise the catalytically active metal in any suitable amount to achieve the required level of activity. Typically, the catalyst comprises the active metal in an amount in the range of from 0.01 to 20% by weight, preferably from 0.02 to 10% by weight, more preferably from 0.1 to 7.5% by weight.

10 Hydrogen or a mixture of hydrogen with other gases, prepared by the catalytic partial process of this invention may be particularly suitable for use as a combustible fuel, either directly or indirectly.

15 The preferred process is suitably used to prepare hydrogen from any hydrocarbonaceous feedstock, especially for the on-board production of hydrogen in fuel cell powered transport means, such as automotive vehicles and crafts.

20 Accordingly, the present invention also relates to transport means provided with the reactor of this invention.

C L A I M S

1. A reactor, suitable for the catalytic conversion of a feed mixture which is capable of explosion or ignition, which reactor comprises a feed supply chamber, an effluent discharge chamber, a catalyst bed having an upstream surface and a downstream surface which is in fluid communication with the effluent discharge chamber, and means for covering part of the upstream surface that partly confine the feed supply chamber, wherein the feed supply chamber has, during normal operation, no zones where the fluid flow is stagnant.
2. A reactor according to claim 1, wherein the uncovered area of the upstream surface can be varied between a maximum and a minimum value, wherein the ratio between the maximum and the minimum value is at least 5, preferably at least 10, more preferable at least 20.
3. A reactor according to claim 1 or 2, wherein the feed supply chamber is equipped with means for swirling the feed mixture.
4. A reactor according to any of the preceding claims, wherein the means for covering part of the upstream surface comprise a body which is moveable parallel to the upstream surface of the catalyst bed, the body having a first surface directed to the upstream surface, and a second surface partly confining the feed supply chamber.
5. A reactor according to claim 4, wherein the means for covering part of the upstream surface comprise two bodies.
6. A reactor according to any of claims 1 to 5, wherein the feed supply chamber has a flow defining surface having an angle with the upstream surface of the catalyst

bed which is smaller than 70° , preferably smaller than 60° , more preferably smaller than 45° .

7. A reactor according to claim 6, wherein the feed supply chamber further has a flow guiding surface that is substantially parallel to the flow defining surface.

8. A reactor according to any of claims 1 to 7, wherein the catalyst bed comprises a catalyst-containing cylindrical arrangement having an inner surface and an outer surface.

9. A reactor according to claim 8, wherein the inner surface of the cylindrical arrangement is the upstream surface of the catalyst bed.

10. A reactor according to claim 3, wherein the means for covering part of the upstream surface comprise a rotatable disc having an axis of rotation parallel to and excentric with respect to the central longitudinal axis of the catalyst bed, which disc has a radius which is larger than the sum of the radius of the catalyst bed and the distance between the longitudinal axis of the catalyst bed and the axis of rotation of the disc, and which disc has at least one opening excentric to the axis of rotation.

11. A reactor according to claim 10, wherein the distance between the centre of the opening and the rotation axis of the disc is equal to the distance between the longitudinal axis of the catalyst bed and the rotation axis of the disc.

12. A reactor according to any of claims 1 to 3, wherein the means for covering part of the upstream surface comprise a flexible wall having a surface that partly defines the feed supply chamber and which surface is capable of partly covering the upstream surface.

13. A process for the catalytic conversion of a fluid feed mixture which is capable of ignition or explosion, wherein the fluid feed mixture is contacted with a

catalyst bed retained in the reactor according to any of claims 1 to 12.

5 14. A process according to claim 13 which is a process for the catalytic partial oxidation of a hydro-carbonaceous feedstock, which process comprises contacting a feed mixture comprising the hydro-carbonaceous feedstock and an oxygen-containing gas with a catalyst bed retained in the reactor according to any of claims 1 to 12.

10 15. Transport means provided with the reactor according to any of claims 1 to 12.

Fig.1.

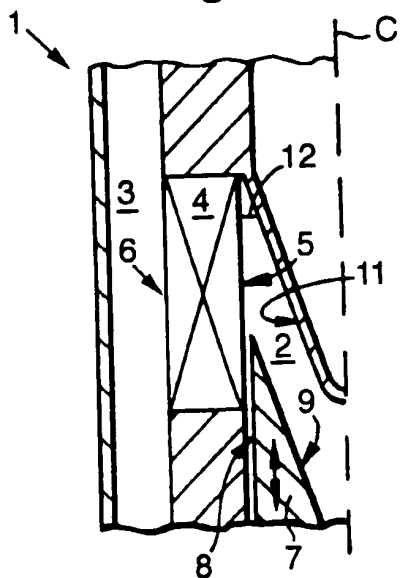


Fig.2.

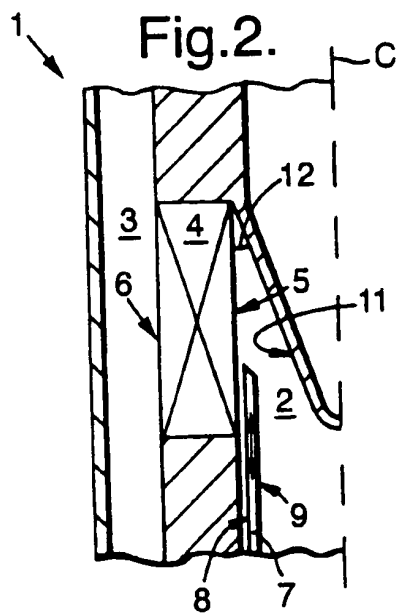


Fig.3.

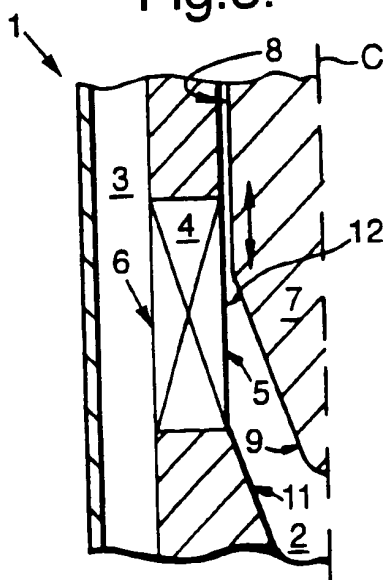


Fig.4.

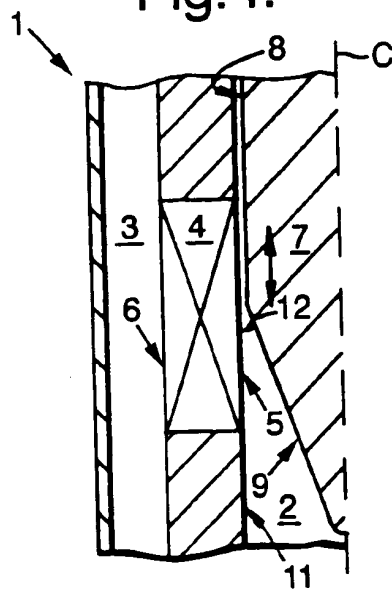


Fig.5a.

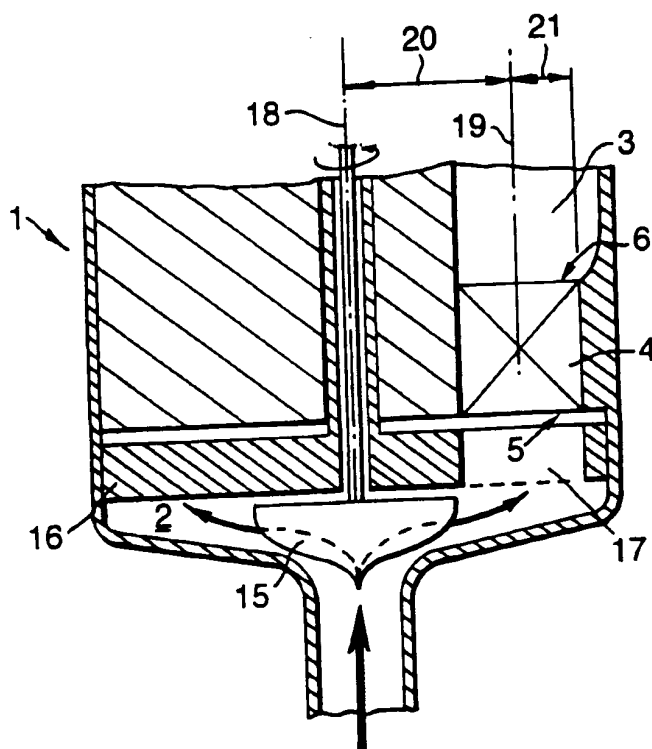


Fig.5b.

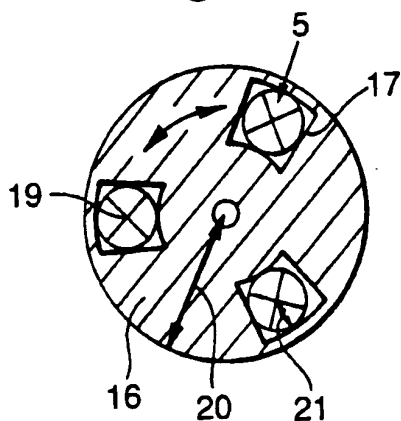


Fig.5c.

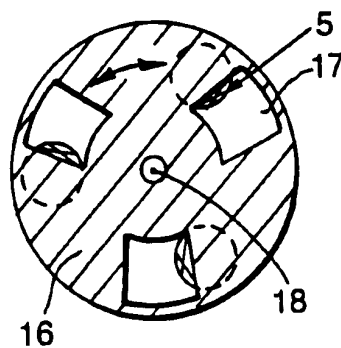


Fig.7c.

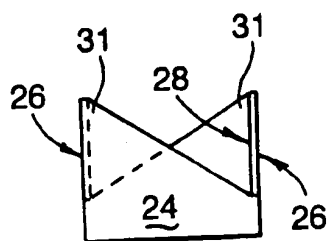


Fig.7d.

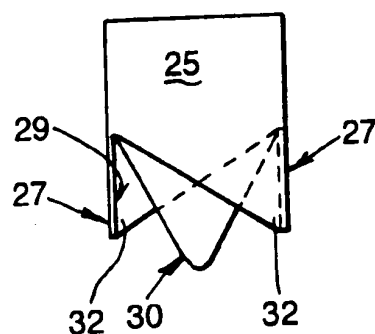


Fig.6a.

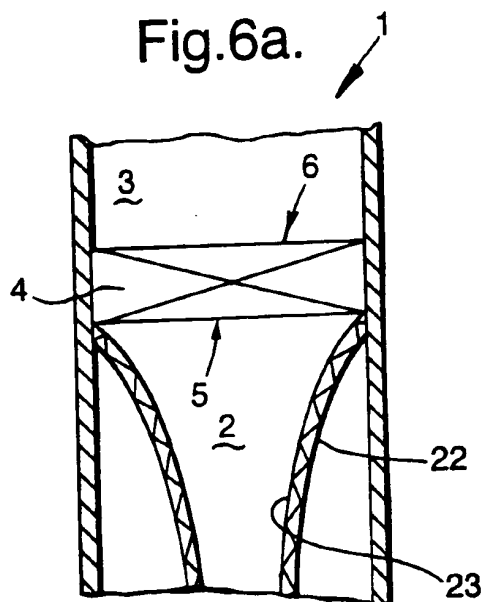


Fig.6b.

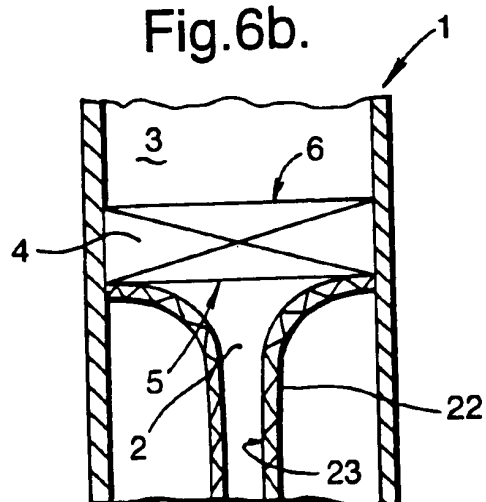


Fig.7a.

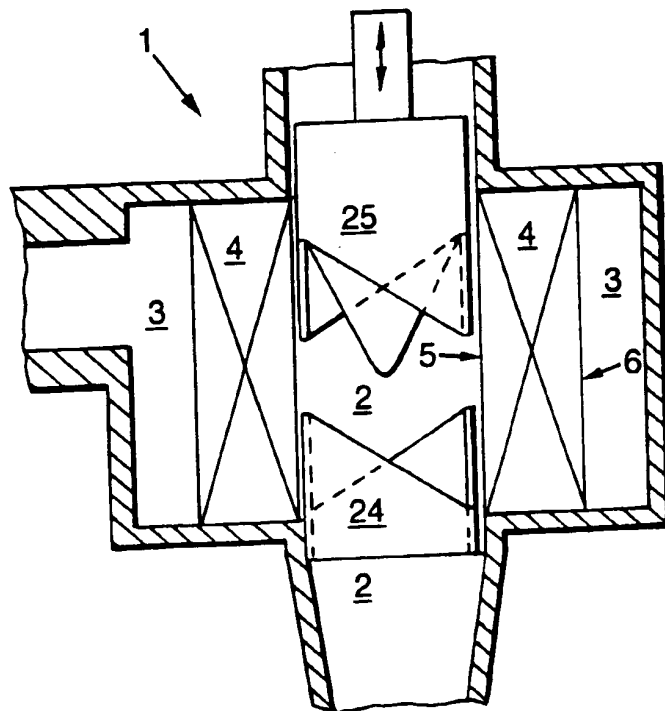
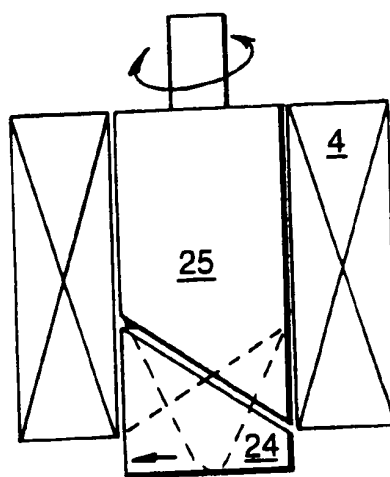


Fig.7b.



INTERNATIONAL SEARCH REPORT

Inventor: and Application No

PCT/EP 99/10447

A. CLASSIFICATION OF SUBJECT MATTER
IPC 7 B01J8/00 B01J8/02

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B01J F02M H01M C01B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the International search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

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X	DE 92 02 798 U (EMITEC GESELLSCHAFT FÜR EMISSIONSTECHNOLOGIE MBH) 23 April 1992 (1992-04-23) figure 6 page 13, line 25 -page 14, line 2 page 8, paragraph 30 -page 9, line 22 page 6, line 25 -page 7, line 12 page 3, line 35 -page 4, line 17 page 1, line 5 - line 28	1,2,4-6, 8,12-15
X	GB 2 303 860 A (DAIMLER-BENZ AG) 5 March 1997 (1997-03-05) figures 3-5 page 12, paragraph 2 -page 13, paragraph 1 page 10, paragraph 3 -page 11, paragraph 1 page 6, paragraph 1 -page 7, paragraph 1 -/-	1,2,4,8, 10,11, 13,15

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

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Date of the actual completion of the international search

4 April 2000

Date of mailing of the international search report

13/04/2000

Name and mailing address of the ISA

European Patent Office, P.B. 5018 Patentamt 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 851 epo nl,
Fax (+31-70) 340-3016

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Stevnsborg, N

INTERNATIONAL SEARCH REPORT

Inventor: and Application No
PCT/EP 99/10447

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